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**STUDY OF THERMAL BUOYANCY AND CONCENTRATION
BUOYANCY EFFECTS ON THE ELECTRICALLY CONDUCTING
FLUID FLOW PAST AN IMPULSIVELY STARTED VERTICAL
PLATE WITH VARIABLE TEMPERATURE AND MASS
DIFFUSION IN THE PRESENCE OF INCLINED MAGNETIC
FIELD.**

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Abstract

Thermal buoyancy and concentration buoyancy effects of the conducting fluid past an impulsively started vertical plate with variable temperature and mass diffusion in the presence of inclined magnetic field is studied in this investigation. Assuming the fluid is gray, absorbing heat and emitting radiation in a non-scattering medium. The dimensional governing partial differential equations obtained in this investigation are converted to non-dimensional partial differential equations and are solved by using Laplace-transform technique subject to the respective boundary conditions. The graphical results are depicted for velocity, temperature and concentration profiles for various existing parameters and time in this discussion. The skin friction for different magnetic parameter, Prandtl number, Schmidt number, thermal Grashof number and mass Grashof number.

Keywords : *Unsteady flow, Vertical plate, Conducting fluid, Magnetic field, Heat transfer, Mass transfer.*

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1. Introduction

During recent years, simultaneous study of conducting fluid flow with heat and mass transfer in presence of magnetic field in different geometries and in various modelling have been observed to play an important role in many engineering and geophysical applications, chemical reaction and biological Science. Some important applications are cooling of nuclear reactors, Liquid metals fluid, power generation system and aerodynamics. The response of laminar skin friction and heat transfer to fluctuations in the stream velocity was first studied by Lighthill [1.]. The free convection effects on the oscillatory flow past an infinite vertical porous plate with constant suction was presented by Soundelgekar [2] . Gupta et al.[3] have studied free convection effects on the flow past an accelerated vertical plate in an incompressible dissipative fluid. Mass transfer effects on the flow past an exponentially accelerated vertical plate with constant heat flux was investigated by Jha et al.[4]. An investigation on radiation effects on free convection flow past a semi-infinite vertical plate was presented by Soundelgekar and Takhar [5]. Effects of mass transfer on flow past an impulsively started infinite vertical plate with constant heat flux and chemical reaction was studied by Das et al [6]. Several researchers in these areas on heat transfer and radiation, mass transfer and chemical reaction were investigated in different models. One may refer the works presented by Soundelgekar and Takhar [6] ,Hossain and Takhar [8], Rapit and Perdikis [9] and Muthucumaraswamy et. al [12]. MHD and Radiation effects on moving isothermal vertical plate with variable mass diffusion have been studied by Muthucumaraswamy and Janakiraman [10]. Prasad et al. [11] investigated radiation and mass transfer effects on two V dimensional flow past an impulsively started infinite vertical plate. Furthermore, these types of works in areas of MHD effects on free convection, radiation effects on mixed convection, combined effects of radiation and mass transfer have been studied. It may be inferred the works done by Muthucumaraswamy[12], Rajesh [13] and Rajput and Surendra [14]. In the present investigation, we have considered to discuss the thermal buoyancy and concentration buoyancy effects on the electrically conducting fluid flow past an impulsively started vertical plate with variable temperature and mass transfer in the presence of inclined magnetic field. The governing partial differential equations have been converted to non-dimensional partial differential equations for momentum, energy and concentration and are solved by using Laplace transform and inverse Laplace transform

technique for different parameters existing in this investigation.

2. Formulation of the Problem

We consider the flow of unsteady, viscous, incompressible electrically conducting fluid past an impulsively started vertical plate. The x -axis is taken along the plate and y -axis is taken perpendicular to the plate. The temperature of the plate and fluid are at the same initially i.e. before starting the motion. An inclined magnetic is applied through the point of intersection of x -axis and y -axis making an angle α in the positive direction of x -axis. The viscous dissipation and induced magnetic field has been ignored due to its less effect. Initially the fluid and plate are at the same temperature T_∞ and concentration C_∞ in the stationary condition. At $t > 0$, the temperature of the plate is raised to T_w and concentration level near the plate is raised to C_w linearly with respect to time. Since the plate is considered in the x -direction, and hence all physical quantities will be independent of x . So under these assumption, the physical variables are purely the function of y and t only.

The mathematical model of the flow is as below

$$\frac{\partial u}{\partial t} = g\beta_t(T - T_\infty) + g\beta_m(C - C_\infty) + \nu \frac{\partial^2 u}{\partial y^2} - \frac{\sigma B_0^2 C \cos^2 \alpha}{\rho} u, \quad (1)$$

$$\frac{\partial T}{\partial t} = \frac{\kappa}{\rho C_p} \frac{\partial^2 T}{\partial y^2}, \quad (2)$$

and

$$\frac{\partial C}{\partial t} = D \frac{\partial^2 C}{\partial y^2}, \quad (3)$$

where u is the velocity of the fluid in x - direction, y - co-ordinate axis normal to the plate, g - acceleration due to gravity, t -time , ρ -density of the fluid, β_t - volumetric coefficient of thermal expansion, β_m -volumetric co-efficient of concentration expansion, σ -electrical conductivity of the fluid(Stefan Boltzmann constant), ν -kinematics viscosity, T_∞ -temperature of the fluid near the plate, C -species concentration in the fluid, T -temperature of the fluid far from the plate, C_∞ -concentration in the fluid far away from the plate, B_0 -external magnetic field, κ -thermal conductivity of the fluid, C_p specific heat at constant pressure and D -mass diffusion.

The boundary conditions for the above governing equations are as follows

$$\left. \begin{aligned} t \leq 0 : u = 0, T = T_\infty, C = C_\infty, \text{ for all values of } y \text{ i.e. } \forall y \\ t > 0 : u = u_0, T = T_\infty + (T_w - T_\infty) \frac{u_0^2 t}{\nu}, C = C_\infty + (C_w - C_\infty) \frac{u_0^2 t}{\nu}, \text{ at } y = 0, \\ u \rightarrow u_0, T \rightarrow T_\infty, C \rightarrow C_\infty \text{ as } y \rightarrow \infty. \end{aligned} \right\} \quad (4)$$

Introducing the following non-dimensional quantities

$$\left. \begin{aligned} \bar{y} = \frac{yu_0}{\nu}, \bar{u} = \frac{u}{u_0}, \theta = \frac{T-T_\infty}{T_w-T_\infty}, \phi = \frac{C-C_\infty}{C_w-C_\infty}, \bar{t} = \frac{tu_0^2}{\nu}, \\ M = \frac{\sigma B_0^2 \nu}{\rho u_0^2}, P_r = \frac{\mu C_p}{\kappa}, S_c = \frac{\nu}{D}, G_r = \frac{g \beta t \nu (T_w - T_\infty)}{u_0^3}, G_c = \frac{g \beta_m \nu (C_w - C_\infty)}{u_0^3}. \end{aligned} \right\} \quad (5)$$

Using equation (5) in equations(1)-(3) we get the respective following non- dimensional equation of momentum, energy and concentration of the conducting fluid as

$$\frac{\partial \bar{u}}{\partial \bar{t}} = \frac{\partial^2 \bar{u}}{\partial \bar{y}^2} + G_r \theta + G_m \phi - (M \cos^2 \alpha) \bar{u}, \quad (6)$$

$$\frac{\partial \bar{\theta}}{\partial \bar{t}} = \frac{1}{P_r} \frac{\partial^2 \bar{\theta}}{\partial \bar{y}^2} \quad (7)$$

and

$$\frac{\partial \bar{\phi}}{\partial \bar{t}} = \frac{1}{S_c} \frac{\partial^2 \bar{\phi}}{\partial \bar{y}^2}. \quad (8)$$

Subject to the following boundary conditions

$$\left. \begin{aligned} \bar{t} \leq 0 : \bar{u} = 0, \theta = 0, \phi = 0, \text{ for all vaules of } \bar{y} \text{ i.e. } \forall \bar{y} \\ \bar{t} > 0 : \bar{u} = 1, \theta = \bar{t}, \phi = \bar{t} \text{ at } \bar{y} = 0, \\ \bar{u} \rightarrow 0, \theta \rightarrow 0, \phi \rightarrow 0 \text{ as } \bar{y} \rightarrow \infty. \end{aligned} \right\} \quad (9)$$

If we drop bars in the afore said non dimensional equations, we have

$$\frac{\partial u}{\partial t} = \frac{\partial^2 u}{\partial y^2} + G_r \theta + G_m \phi - (M \cos^2 \alpha) u, \quad (10)$$

$$\frac{\partial \theta}{\partial t} = \frac{1}{P_r} \frac{\partial^2 \theta}{\partial y^2} \quad (11)$$

and

$$\frac{\partial \phi}{\partial t} = \frac{1}{S_c} \frac{\partial^2 \phi}{\partial y^2}. \quad (12)$$

with the following appropriate boundary conditions

$$\left. \begin{aligned} t \leq 0 : u = 0, \theta = 0, \phi = 0, \quad \text{for all values of } y \text{ i.e. } \forall y \\ t > 0 : u = 1, \theta = t, \phi = t \quad \text{at } y = 0, \\ u \rightarrow 0, \theta \rightarrow 0, \phi \rightarrow 0 \quad \text{as } y \rightarrow \infty. \end{aligned} \right\} \quad (13)$$

The non-dimensional governing equations (10)-(12) subject to the boundary conditions (13) have been solved by using usual Laplace transform technique along with the help of B. Hetnarskis [15] development made on Laplace transform and inverse Laplace transform technique.

First of all, using Laplace transform technique in concentration equation (12), we have

$$L\left\{\frac{\partial\phi(y,t)}{\partial t}\right\} = L\left\{\frac{1}{S_c}\frac{\partial^2\phi(y,t)}{\partial y^2}\right\},$$

which implies

$$sL\{\phi(y,t)\} - \phi(y,0) = \frac{1}{S_c}L\left\{\frac{\partial^2\phi(y,t)}{\partial y^2}\right\}. \quad (14)$$

Using the boundary conditions (13) in (14) we get,

$$\frac{d^2L\{\phi(y,t)\}}{dy^2} - sS_cL\{\phi(y,t)\} = 0,$$

which gives the solution as below

$$L\{\phi(y,t)\} = A_1e^{y\sqrt{sS_c}} + A_2e^{-y\sqrt{sS_c}}, \quad (15)$$

where A_1 and A_2 are arbitrary constants.

Again using the boundary conditions (13), we get

$$L\{\phi(y,t)\} = L\{t\} = \frac{1}{s^2} = A_1 + A_2. \quad (16)$$

Since $\phi(y,t)$ is bounded for $y \rightarrow \infty$, so $\phi(y,s)$ is also bounded as $y \rightarrow \infty$ which implies that we must choose A_1 as Spiegel, M. R. Spiegel[16] Page 97

$$L\{\phi(y,t)\} = L\{0\} = 0 = A_1. \quad (17)$$

Using equations (16) and (17), in equation (15) gives the following solution

$$L\{\phi(y,t)\} = \frac{1}{s^2}e^{-y\sqrt{sS_c}}. \quad (18)$$

Using inverse Laplace transform technique, we get,

$$\begin{aligned}\phi(y, t) &= L^{-1} \left\{ \frac{1}{s^2} e^{-y\sqrt{sS_c}} \right\}, \\ \Rightarrow \phi(y, t) &= \left(t + \frac{y^2 S_c}{2} \operatorname{erfc} \left(\frac{y\sqrt{S_c}}{2\sqrt{t}} \right) \right) - \frac{y\sqrt{S_c t}}{\sqrt{\pi}} e^{-\frac{y^2 S_c}{4t}}.\end{aligned}\quad (19)$$

Again transforming the equation (11) and using the boundary (13), we get

$$\frac{d^2 L\{\theta(y, t)\}}{dy^2} - sP_r L\{\theta(y, t)\} = 0,$$

whose solution gives after using boundary conditions(13) as follows.

$$L\{\theta(y, t)\} = A_3 e^{y\sqrt{sP_r}} + A_4 e^{-y\sqrt{sP_r}},$$

A_3 and A_4 are arbitrary constants.

Using (13), values of A_3 and A_4 may be calculated as $A_3 = 0$ and $A_4 = \frac{1}{s^2}$ which implies

$$L\{\theta(y, t)\} = \frac{1}{s^2} e^{-y\sqrt{sP_r}}. \quad (20)$$

Now taking inverse Laplace transform, we get

$$\theta(y, t) = \left(t + \frac{y^2 P_r}{2} \operatorname{erfc} \left(\frac{y\sqrt{P_r}}{2\sqrt{t}} \right) \right) - \frac{y\sqrt{P_r t}}{\sqrt{\pi}} e^{-\frac{y^2 P_r}{4t}}. \quad (21)$$

Again taking Laplace transform on both sides of equation (10), we have

$$L \left\{ \frac{\partial u(y, t)}{\partial t} \right\} = L \left\{ \frac{\partial^2 u(y, t)}{\partial y^2} + G_r \theta(y, t) + G_m \phi(y, t) - (M \cos^2 \alpha) u(y, t) \right\}.$$

which implies $sL\{u(y, t)\} - u(y, 0)$

$$= \frac{d^2 L\{u(y, t)\}}{dy^2} - (M \cos^2 \alpha) L\{u(y, t)\} + G_r L\{\theta(y, t)\} + G_m L\{\phi(y, t)\}. \quad (22)$$

Using the boundary conditions (13), equation (22) gives

$$\frac{d^2 L\{u(y, t)\}}{dy^2} - (s + M \cos^2 \alpha) L\{u(y, t)\} = -G_r L\{\theta(y, t)\} - G_m L\{\phi(y, t)\}. \quad (23)$$

The general solution of (23) will be of the form

$$L\{u(y, t)\} = A.E. + P.I. \quad (24)$$

with

$$A.E. = A_5 e^{y\sqrt{s+M\cos^2\alpha}} + A_6 e^{-y\sqrt{s+M\cos^2\alpha}},$$

and A_5 and A_6 are arbitrary constants and

$$P.I. = -G_r \frac{1}{D^2 - s + M_1} L\{\theta(y, t)\} - G_m \frac{1}{D^2 - s + M_1} L\{\phi(y, t)\}$$

where $M_1 = M \cos^2 \alpha$. Substituting the value of $L\{\phi(y, t)\}$ and $L\{\theta(y, t)\}$ from equation (18) and (20) respectively, equation (24) becomes

$$L\{u(y, t)\} = A_5 e^{y\sqrt{s+M\cos^2\alpha}} + A_6 e^{-y\sqrt{s+M\cos^2\alpha}} + \frac{G_r}{(1-P_r)} \frac{e^{-y\sqrt{sP_r}}}{s^2(s-a)} + \frac{G_m}{(1-S_c)} \frac{e^{-y\sqrt{sS_c}}}{s^2(s-b)}, \quad (25)$$

where $a = \frac{M_1}{P_r-1}$ and $b = \frac{M_1}{S_c-1}$.

Taking inverse Laplace transform of equation (25) and using boundary conditions (13) yields

$$\frac{1}{a} = A_5 + A_6 + \frac{G_r}{(1-P_r)s^2(s-a)} + \frac{G_m}{(1-S_c)s^2(s-b)}.$$

When $y \rightarrow \infty$, $u(y, t) \rightarrow 0$, so $L\{u(y, t)\} \rightarrow 0$ for $y \rightarrow \infty$ and hence $L\{u(y, t)\}$ is bounded for being $u(y, t)$ is bounded when $y \rightarrow \infty$. So $A_5 = 0$ and

$$A_6 = \frac{1}{s} - \frac{G_r}{(1-P_r)s^2(s-a)} - \frac{G_m}{(1-S_c)s^2(s-b)}.$$

Hence equation (25) becomes

$$\begin{aligned} L\{u(y, t)\} &= \frac{1}{s} e^{-y\sqrt{s+M_1}} + \\ &\frac{G_r}{(1-P_r)} \frac{(e^{-y\sqrt{sP_r}} - e^{-y\sqrt{s+M_1}})}{s^2(s-a)} \\ &+ \frac{G_m}{(1-S_c)} \frac{(e^{-y\sqrt{sS_c}} - e^{-y\sqrt{s+M_1}})}{s^2(s-b)}. \end{aligned} \quad (26)$$

Taking inverse Laplace transform of (26) and with the help of Article by Hetnarski,

R.B. [15] the solutions are derived as below.

$$\begin{aligned}
u(y, t) = & B_1 e^{-y\sqrt{M_1}} \operatorname{erfc} \left(\frac{y}{2\sqrt{t}} - \sqrt{M_1 t} \right) + B_2 e^{y\sqrt{M_1}} \operatorname{erfc} \left(\frac{y}{2\sqrt{t}} + \sqrt{M_1 t} \right) \\
& - G_3 \operatorname{erfc} \left(\frac{y\sqrt{P_r}}{2\sqrt{t}} \right) - G_4 \operatorname{erfc} \left(\frac{y\sqrt{S_c}}{2\sqrt{t}} \right) + G_5 \left\{ e^{-y\sqrt{aP_r}} \operatorname{erfc} \left(\frac{y}{2\sqrt{t}} - \sqrt{at} \right) \right. \\
& + e^{y\sqrt{aP_r}} \operatorname{erfc} \left(\frac{y}{2\sqrt{t}} + \sqrt{at} \right) + e^{-y\sqrt{a+M_1}} \operatorname{erfc} \left(\frac{y}{2\sqrt{t}} - \sqrt{(a+M_1)t} \right) \\
& \left. + e^{y\sqrt{a+M_1}} \operatorname{erfc} \left(\frac{y}{2\sqrt{t}} + \sqrt{(a+M_1)t} \right) \right\} \\
& + G_6 \left\{ e^{-y\sqrt{bS_c}} \operatorname{erfc} \left(\frac{y}{2\sqrt{t}} - \sqrt{bt} \right) + e^{y\sqrt{bS_c}} \operatorname{erfc} \left(\frac{y}{2\sqrt{t}} + \sqrt{bt} \right) \right\} \\
& - G_6 \left\{ e^{-y\sqrt{b+M_1}} \operatorname{erfc} \left(\frac{y}{2\sqrt{t}} - \sqrt{(b+M_1)t} \right) + e^{y\sqrt{b+M_1}} \operatorname{erfc} \left(\frac{y}{2\sqrt{t}} + \sqrt{(b+M_1)t} \right) \right\} \\
& - G_7 \left\{ t + \frac{y^2 P_r}{2} \operatorname{erfc} \left(\frac{yP_r}{2\sqrt{t}} \right) - \frac{y\sqrt{P_r t}}{\sqrt{\pi}} e^{-\frac{y^2 P_r}{4t}} \right\} \\
& - G_8 \left\{ t + \frac{y^2 S_c}{2} \operatorname{erfc} \left(\frac{yS_c}{2\sqrt{t}} \right) - \frac{y\sqrt{S_c t}}{\sqrt{\pi}} e^{-\frac{y^2 S_c}{4t}} \right\} \tag{27}
\end{aligned}$$

where

$$G_1 = 1 + G_3 + G_4, \quad G_2 = G_7 + G_8, \quad G_3 = \frac{G_r}{a^2(1-P_r)}, \quad G_4 = \frac{G_m}{b^2(1-S_c)},$$

$$G_5 = \frac{G_3}{2} e^{at}, \quad G_6 = \frac{G_4}{2} e^{bt}, \quad G_7 = \frac{G_r}{a(1-P_r)}, \quad G_8 = \frac{G_m}{b(1-S_c)},$$

$$B_1 = \frac{1}{2} \left[G_1 + G_2 \left(t - \frac{y}{2\sqrt{M_1}} \right) \right], \quad B_2 = \frac{1}{2} \left[G_1 + G_2 \left(t + \frac{y}{2\sqrt{M_1}} \right) \right].$$

Skin friction, Nusselt number and Sherwood number : In this paper, we consider the physical quantities of interaction which are known as the Skin friction co-efficient C_f , the Nusselt number N_u and the Shewood number S_h which are defined as $N_u = \frac{\nu q_w}{u_0 \kappa (T_w - T_\infty)}$ and $S_h = \frac{\nu j_w}{u_0 D (C_w - C_\infty)}$ respectively where τ_w is the skin friction or shear stress, q_w and j_w are the heat and mass flux from the plate which are given by $\tau_w = -\mu \left(\frac{\partial u}{\partial y} \right)_{y=0}$, $q_w = -\alpha \left(\frac{\partial T}{\partial y} \right)_{y=0}$, and $j_w = -D \left(\frac{\partial C}{\partial y} \right)_{y=0}$, respectively.

Using the non-dimensionless variables (5) the dimensionless physical parameters skin-friction coefficient, Nusselt number and Sherwood number are found as below

Skin frictionco efficient :

$$\begin{aligned}
\tau_w = & \frac{1}{2M^2}\sqrt{M}(erfc\sqrt{Mt} - 2)G_r(P_r - 1) + \frac{1}{2M^2}G_m(S_c - 1) + \frac{t(G_m + G_r)}{2M} \\
& + \frac{1}{4M\sqrt{M}}(G_m + G_r)(erfc\sqrt{Mt} - 2) + G_r\sqrt{\frac{P_r t}{\pi}} + \frac{t}{M}\sqrt{\frac{P_r}{\pi t}} + G_m\sqrt{\frac{S_c t}{\pi}} \\
& + \frac{t}{M}\sqrt{\frac{S_c}{\pi t}} + \frac{1}{2M^2}\sqrt{M}erfc\sqrt{Mt}G_r(P_r - 1) + \frac{t(G_m + G_r)}{2M} \\
& + \frac{1}{4M\sqrt{M}}(G_m + G_r)erfc\sqrt{Mt} - \frac{1}{2M^2}G_r(P_r - 1)e^{-Mt} + \frac{1}{2M^2}G_m(S_c - 1) \\
& + \frac{t(G_m + G_r)}{2M\sqrt{\pi t}} - \frac{1}{2M^2}G_r(P_r - 1)e^{-Mt} + \frac{t(G_m + G_r)}{2M\sqrt{\pi t}} \\
& + \frac{1}{2M^2}\left[G_re^{-\frac{Mt}{P_r-1}}(P_r - 1)erfc\left(\sqrt{t\left(M + \frac{M}{P_r - 1}\right)}\right)\sqrt{\left(M + \frac{M}{P_r - 1}\right)}\right. \\
& + \left\{erfc\left(\sqrt{t\left(M + \frac{M}{P_r - 1}\right)}\right) - 2\right\}\sqrt{\left(M + \frac{M}{P_r - 1}\right)} \\
& \left. - \frac{2e^{-t\left(M + \frac{M}{P_r - 1}\right)}}{\sqrt{\pi t}}\right] - \frac{1}{2M^2}\left[G_me^{-\frac{Mt}{S_c-1}}\right. \\
& \left. erfc\left(\sqrt{t\left(M + \frac{M}{S_c - 1}\right)}\right)\sqrt{\left(M + \frac{M}{S_c - 1}\right)} + \left\{\left(\sqrt{t\left(M + \frac{M}{S_c - 1}\right)}\right) - 2\right\}\right. \\
& \left.\sqrt{\left(M + \frac{M}{P_r - 1}\right)} - \frac{2e^{-t\left(M + \frac{M}{S_c - 1}\right)}}{\sqrt{\pi t}}\right] \\
& + \frac{1}{2M^2}\left[G_re^{-\frac{Mt}{P_r-1}}(P_r - 1)\left\{erfc\left(\sqrt{\frac{Mt}{P_r - 1}}\right) - 2\right\}\right. \\
& \left.\sqrt{\frac{MP_r}{P_r - 1}} + erfc\left(\sqrt{\frac{Mt}{P_r - 1}}\right) - 2\frac{e^{-\frac{Mt}{P_r-1}}}{\sqrt{\pi t}}\right] \\
& + \frac{1}{2M^2}\left[G_me^{-\frac{Mt}{S_c-1}}(S_c - 1)\left\{\left(\sqrt{\frac{Mt}{S_c - 1}}\right) - 2\right\}\right. \\
& \left.\sqrt{\frac{Mt}{S_c - 1}} + erfc\left(\sqrt{\frac{Mt}{S_c - 1}}\right)\sqrt{\frac{MS_c}{S_c - 1}} - 2\frac{e^{-\frac{Mt}{S_c-1}}}{\sqrt{\pi t}}\right] \\
& + \frac{G_r(P_r - 1)\sqrt{P_r}}{M^2\sqrt{\pi t}} + \frac{G_m(S_c - 1)\sqrt{S_c}}{M^2\sqrt{\pi t}}
\end{aligned} \tag{28}$$

Nusselt number :

$$Nu = -\sqrt{\frac{Pr t}{\pi}} \quad (29)$$

Sherwood number :

$$Sh = -\sqrt{\frac{Sc t}{\pi}} \quad (30)$$

Table 1 : Effects of magnetic parameter M on Skin friction, Nusselt number and Sherwood number for $Pr = 1.2, Sc = 1.5, G_m = 2, t = 0.5, G_r = 1$

M	τ_w	Nu	Sh
0.5	13.7897	0.6308	0.4370
1	6.4596	0.6308	0.4370
2	4.2994	0.6308	0.4370
3	4.0184	0.6308	0.4370

Table 2 : Effects of Prandtl number Pr on Skin friction, Nusselt number and Sherwood number for $M = 2, Sc = 1.5, G_m = 2, t = 0.5, G_r = 1$.

Pr	τ_w	Nu	Sh
1.4	8.2211	0.4720	0.4370
2	4.4320	0.5642	0.4370
2.5	4.2994	0.6308	0.4370
7	5.3796	1.0555	0.4370

Table 3 : Effects of Schmidt number Sc on Skin friction, Nusselt number and Sherwood number for $Pr = 1.2, M = 2, G_m = 2, t = 0.5, G_r = 1$.

Sc	τ_w	Nu	Sh
1.2	4.2994	0.6308	0.4370
2	4.0991	0.6308	0.5642
3	3.6403	0.6308	0.6910
4	2.9946	0.6308	0.7979

Table 4 : Effects of thermal buoyancy parameter G_r on Skin friction, Nusselt number and Sherwood number for $P_r = 1.2, S_c = 1.5, G_m = 2, t = 0.5, M = 2$.

1	4.2994	0.6308	0.4370
2	6.9276	0.6308	0.4370
5	14.8122	0.6308	0.4370

Table 5 : Effects of concentration buoyancy parameter G_m on Skin friction, Nusselt number and Sherwood number for $P_r = 1.2, S_c = 1.5, M = 2, t = 0.5, G_r = 1$.

G_m	τ_w	Nu	Sh
1	4.1887	0.6308	0.4370
2	4.2994	0.6308	0.4370
3	4.4101	0.6308	0.4370
5	4.6315	0.6308	0.4370

Table 6 : Effects of time t on Skin friction, Nusselt number and Sherwood number for $P_r = 1.2, S_c = 1.5, G_m = 2, M = 2, G_r = 1$.

t	τ_w	Nu	Sh
0.1	3.3737	0.2821	0.1954
0.3	3.5633	0.4886	0.3385
0.5	4.2994	0.6308	0.4370
0.7	4.3039	0.7464	0.5171
1	7.3584	0.8921	0.6180

3. Results and Discussion

The values of skin friction coefficient, Nusselt number and Sherwood numbers calculated from (28) - (30) for different existing parameters are tabulated in Table 1-6. It is clearly observed from Table-1 & 3 that magnitude of skin-friction co-efficient decreases as the magnetic parameter M and Schmidt number S_c increase and no magnetic effects are observed on Nusselt and Sherwood number; but with the increase of Schmidt number S_c Sherwood number is seen to increase as shown in Table-3. The magnitude of skin-friction co-efficient also decreases initially with the increase of Prandtl number

P_r and then finally increase for higher value of Prandtl number $P_r > 2.5$. The effect of Prandtl number P_r is seen to increase the Nusselt number in Table-2. The magnitude of skin friction are seen to increase with the increase of thermal buoyancy parameter G_r , concentration buoyancy parameter G_m and time t as shown in the Table-4, Table-5 and Table-6 respectively and no effects are observed in Nusselt number and Sherwood number except time t . It is clearly observed from Table-6 that Skin friction coefficient, Nusselt number and Sherwood number increase with increase of time t .

Numerical evaluations of the results obtained by using Laplace transform technique for the typical profiles of the dimensionless velocity, temperature and concentration of the conducting fluid reported in the preceding section were performed for different existing parameters across the boundary layer. A representative set of graphical results are depicted in Fig.1-10. Fig.1, 2 & 3 demonstrate the typical profiles of the dimensionless velocity for different the magnetic parameter M_1 , different thermal buoyancy parameter G_r and different concentration buoyancy parameter G_m respectively. The effects of magnetic parameter M_1 on the velocity distribution is shown in Fig.1 where velocity of the conducting fluid is seen to decrease with increasing the value of M_1 . This is due to the presence of Lorentz force which retards the motion of the conducting fluid across the boundary layer. Physically, the higher of magnetic parameter M_1 implies the higher of the ponder motive force called Lorentz force which reduces the boundary layer thickness of the conducting fluid. So the velocity decreases with increase in M_1 . It can be clear from Fig.2 & 3 that the effects of both thermal buoyancy parameter G_r and concentration buoyancy parameter G_m on the dimensionless velocity of the conducting fluid are seen to increase across the boundary layer. This is due to the physical point of view as buoyancy force increases in the upward direction and as a result induces more flow along the vertical plate/sheet which causes the velocity of the fluid increase. i.e. assisting the flow in upward direction. This Phenomenon in the flow velocity occurs at the expense of both the temperature and concentration of the conducting fluid across the boundary. Fig.4 represents the temperature profiles for various Prandtl number P_r and it is observed that the effect of Prandtl number P_r is to decrease the temperature of the conducting fluid across the boundary layer. The increase of Prandtl number P_r leads to fall temperature in the temperature of the conducting fluid. The reason is that lower P_r value has more uniform temperature distribution across the boundary layer as

compared to higher P_r value. This Phenomenon occurs only when the lesser values of P_r are equivalent to increasing thermal conductivity. Therefore, heat is capable to diffuse away from the heated surface more quickly compare to bigger values of Prandtl number P_r . Fig.5 depicts the concentration profiles of the conducting fluid for the different Schmidt number S_c . It is obvious from Fig.5 that the effect of increasing values of S_c , results in an decreasing the concentration distribution. That is, concentration boundary layer thickness decreases with increasing the value of Schmidt number S_c . The effect of Prandtl number P_r on the dimensionless profiles is shown in Fig.6. It can be seen that the velocity distribution of the conducting fluid decrease with the increase of P_r . Fig.7 represents the velocity distribution of the conducting fluid across the boundary layer for different Schmidt number S_c . It is seen that the effect of S_c is to decrease the velocity of the conducting fluid. Fig.8, 9 & 10 show the velocity, temperature and concentration for different values of time t respectively. It is clearly shown that with increase of time t ; the velocity, temperature and concentration distribution are also observed to increase across the boundary layer.

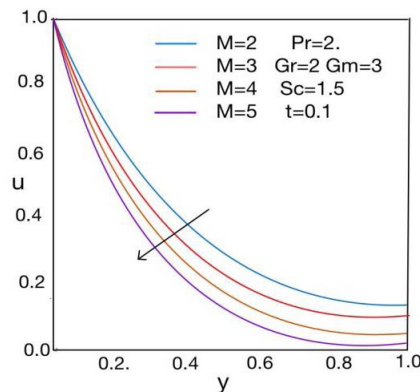


Fig.1 Velocity profiles for different magnetic parameter M

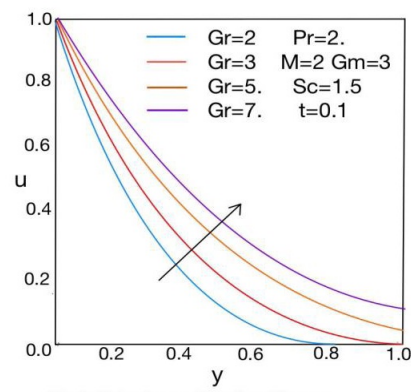


Fig.2 Velocity profiles for different Grashof number Gr

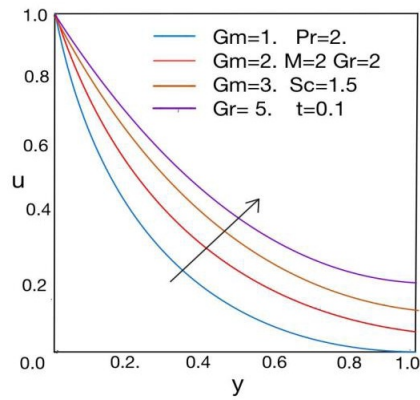


Fig.3 Velocity profiles for different concentration buoyancy parameter Gm

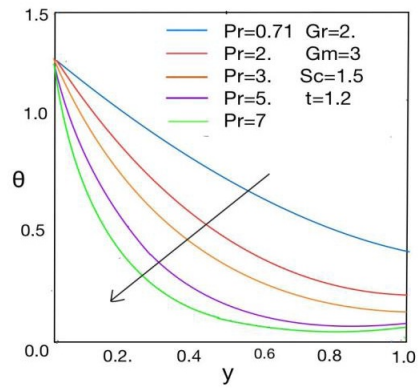


Fig.4 Temperature profiles for different Prandtl number Pr

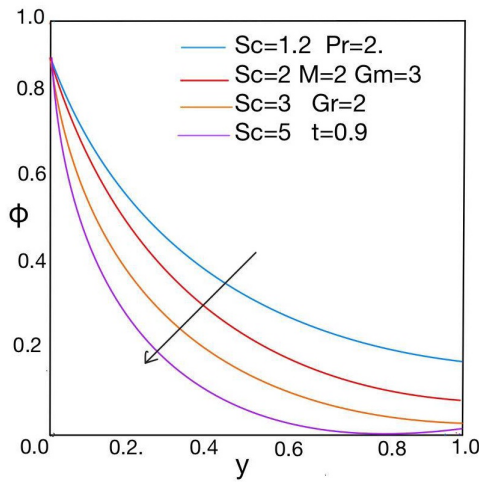


Fig.5 Concentration profiles for different Schmidt number Sc

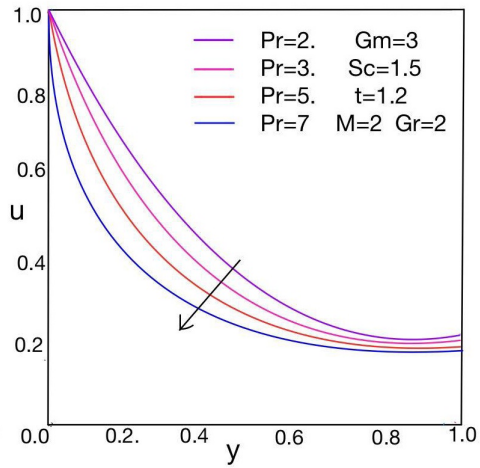


Fig.6 Velocity profiles for different Prandtl number Pr

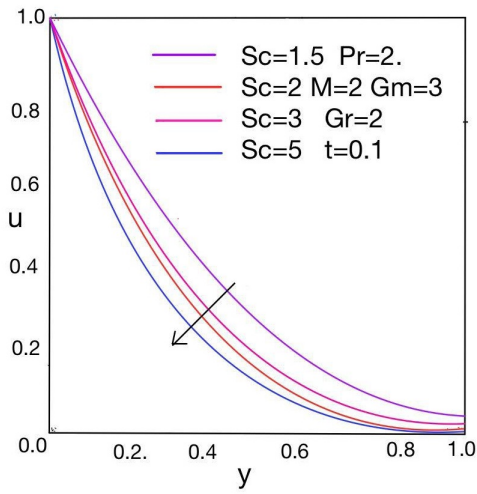


Fig.7 Velocity profiles for different Schmidt number Sc

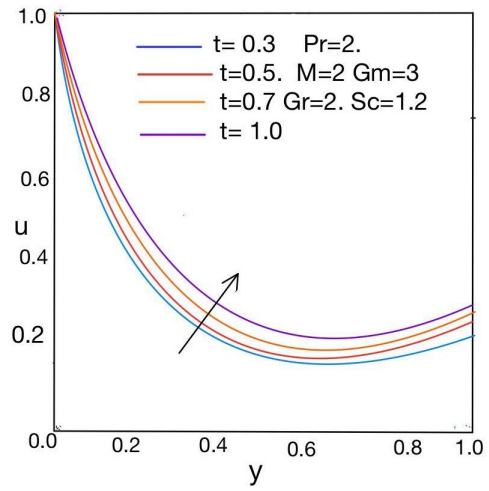


Fig.8 Velocity profiles for different time t.

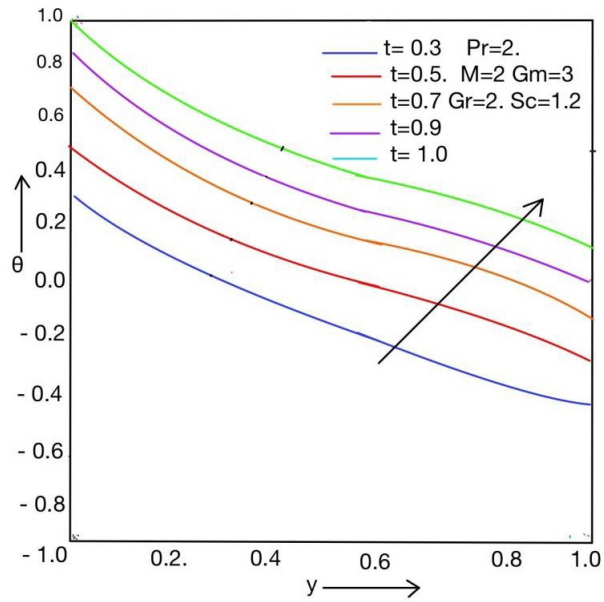


Fig.9 Temperature profiles for different time t.

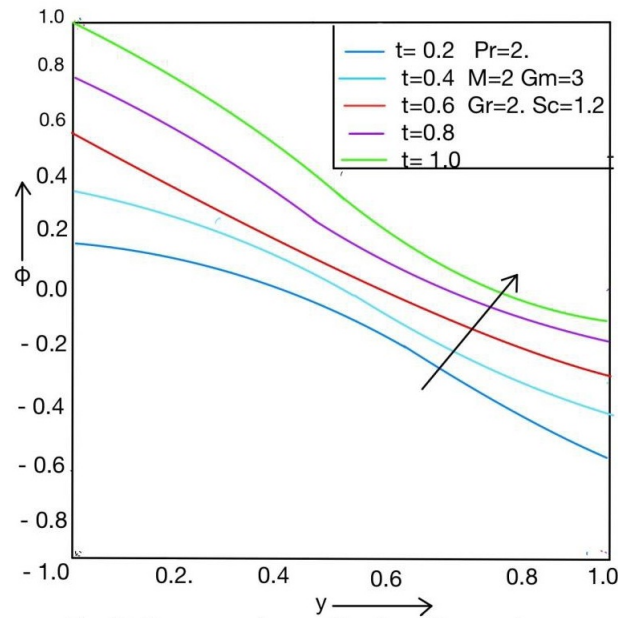


Fig.10 Concentration profiles for different time t .

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